Int'l Appl. No.

PCT/EP2004/009216

Int'l filing date

August 17, 2004

AMENDMENTS TO THE CLAIMS

- 1. (Currently amended) A method for separating mono-branched hydrocarbons from a mixture of hydrocarbons comprising:
 - bringing said mixture into contact with one adsorbent having a selectivity order from mono-branched to linear further to multi-branched hydrocarbons,
 - preferentially and selectively adsorbing said mono-branched hydrocarbons by said adsorbent, and
 - desorbing said mono-branched hydrocarbons from said adsorbent, thereby allowing to-selectively separate separating said mono-branched hydrocarbons.
- 2. (Currently amended) Method-The method according to claim 1 comprising the step of bringing said mixture into contact with only one absorbent.
- 3. (Currently amended) <u>Method A method for separating mixtures of hydrocarbons into fractions of linear, mono-branched and multi-branched hydrocarbons comprises comprising the steps of:</u>
 - a. bringing said mixture into contact with only one adsorbent, said adsorbent having a selectivity order from mono-branched to linear further to multi- branched hydrocarbons,
 - b. separating a stream enriched in multi-branched hydrocarbons from said adsorbent, thereby allowing to separate separating said multi-branched hydrocarbons,
 - c. desorbing the linear hydrocarbons from said adsorbent, thereby allowing to separateseparating said linear hydrocarbons, and
 - d. desorbing said mono-branched hydrocarbons from said adsorbent, thereby allowing to separate separating said mono-branched hydrocarbons.
- 4. (Currently amended) Method The method according to any of claims 1 to 3 claim 1, wherein said hydrocarbons are alkanes.
- 5. (Currently amended) Method The method according to any of claims 1 to 4claim 1, whereby wherein said adsorbent is a zeolitic adsorbent.

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- 6. (Currently amended) Method The method according to any of claims 1 to 5 claim 1, whereby wherein said adsorbent is a zeolitic adsorbent having cavities of which the dimensions are larger than the pore openings giving access to these said cavities, these cavities having a smallest diameter of at least 4.5 Angström and a largest diameter of at least 10 Angström.
- 7. (Currently amended) Method The method according to claim 6, whereby wherein said cavities have a smallest diameter between 4.5 and 15 Angström, and a largest diameter between 10 and 25 Angström.
- 8. (Currently amended) Method The method according to any of claims 1-7claim 5, whereby wherein said zeolitic adsorbent comprises the molar relationship

 X_2O_3 : (n) YO_2

wherein n is at least 2, X is a trivalent element and Y is a tetravalent element.

- 9. (Currently amended) Method-The method according to claim 8, whereby wherein n is at least 2, wherein X is selected from the group comprising consisting of aluminium aluminum, iron, gallium and boron and wherein Y is silicon.
- 10. (Currently amended) Method The method according to claim 8-or 9, whereby wherein n is at least 10, wherein X is aluminium aluminum, and wherein Y is silicon.
- 11. (Currently amended) Method The method according to any of claims 1-10claim 5, whereby wherein said zeolitic adsorbent is MCM- 22.
- 12. (Currently amended) Method The method according to any of claims 1-11 claim 5, wherein said zeolitic adsorbent has a pore occupancy comprised between 0.01 and 100%.

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13. (Currently amended) Method The method according to any of claims 1-12, claim 4 whereby wherein said mixture of alkanes is a mixture of selected from linear, mono-branched and multi-branched alkanes.

- 14. (Currently amended) Method-The method according to claim 13, wherein said mixture comprises 0.1-99. 9% linear, 0.1-99. 9% mono-branched and 0.1-90% multi-branched alkanes.
- 15. (Currently amended) Method The method according to any of claims 13-14claim 13, whereby wherein said mixture of alkanes is a mixture of linear and mono-branched alkanes in a ratio comprised between 1: 100 to 100: 1.
- 16. (Currently amended) Method-The method according to claim 15, wherein said mixture comprises mono-branched and linear alkanes in a ratio of 1: 1.
- 17. (Currently amended) Method The method according to any of claims 1–16claim 1, wherein said separation is based on entropic effects.
- 18. (Currently amended) Use of only one adsorbent A method for separating mono-branched hydrocarbons from a mixture of hydrocarbons which comprises bringing said mixture of hydrocarbons into contact with only one adsorbent.
- 19. (Currently amended) Use of one adsorbent The method according to claim 18 for preferentially adsorbing wherein mono- branched hydrocarbons from said mixture are preferentially adsorbed.
- 20. (Currently amended) Use-The method according to claim 18-or 19, wherein said adsorbent is an adsorbent as defined in any of claims 5-12a zeolitic adsorbent.

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21. (Currently amended) <u>Use The method according to any of claims 18-20claim 18</u>, wherein said mixture is a <u>mixture as defined in any of claims 13-16selected from linear, mono-branched, and multi-branched alkanes</u>.

- 22. (Currently amended) Use-The method according to any of claims 18 21 claim 18, wherein said separation is based on entropic effects.
- 23. (Currently amended) Use of MCM-22 as a zeolite having a catalytic and an adsorbent activity A method for separating mixtures of non-aromatic hydrocarbons into fractions of linear, mono- branched and multi-branched hydrocarbons which comprises contacting said mixture with MCM-22 as a zeolite having a catalytic and an adsorbent activity.